

# Synthesis of Cost Effective and Sustainable Pathways to Wastewater Treatment

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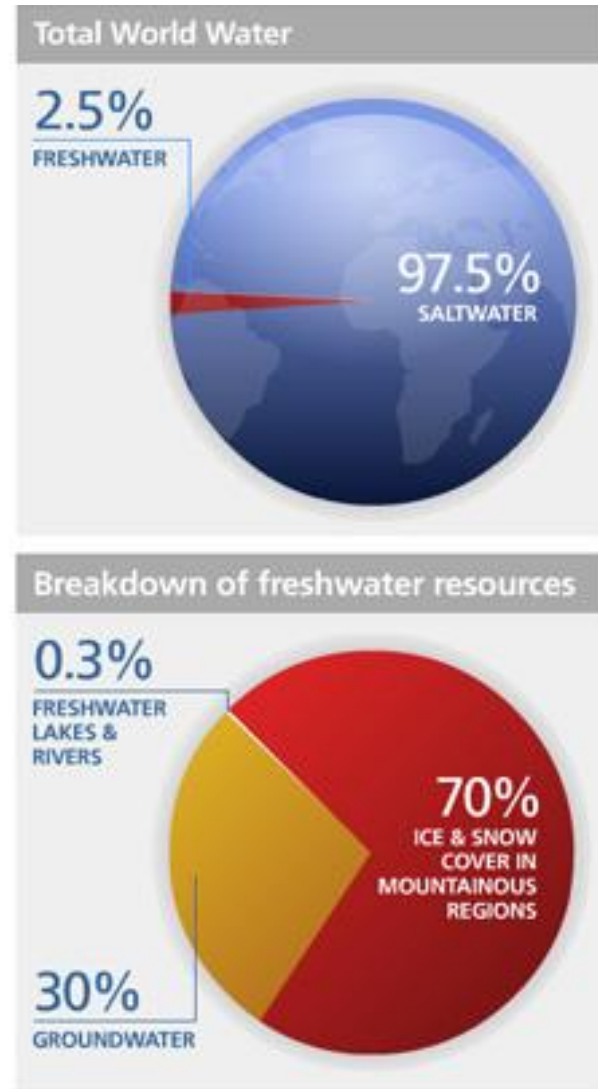
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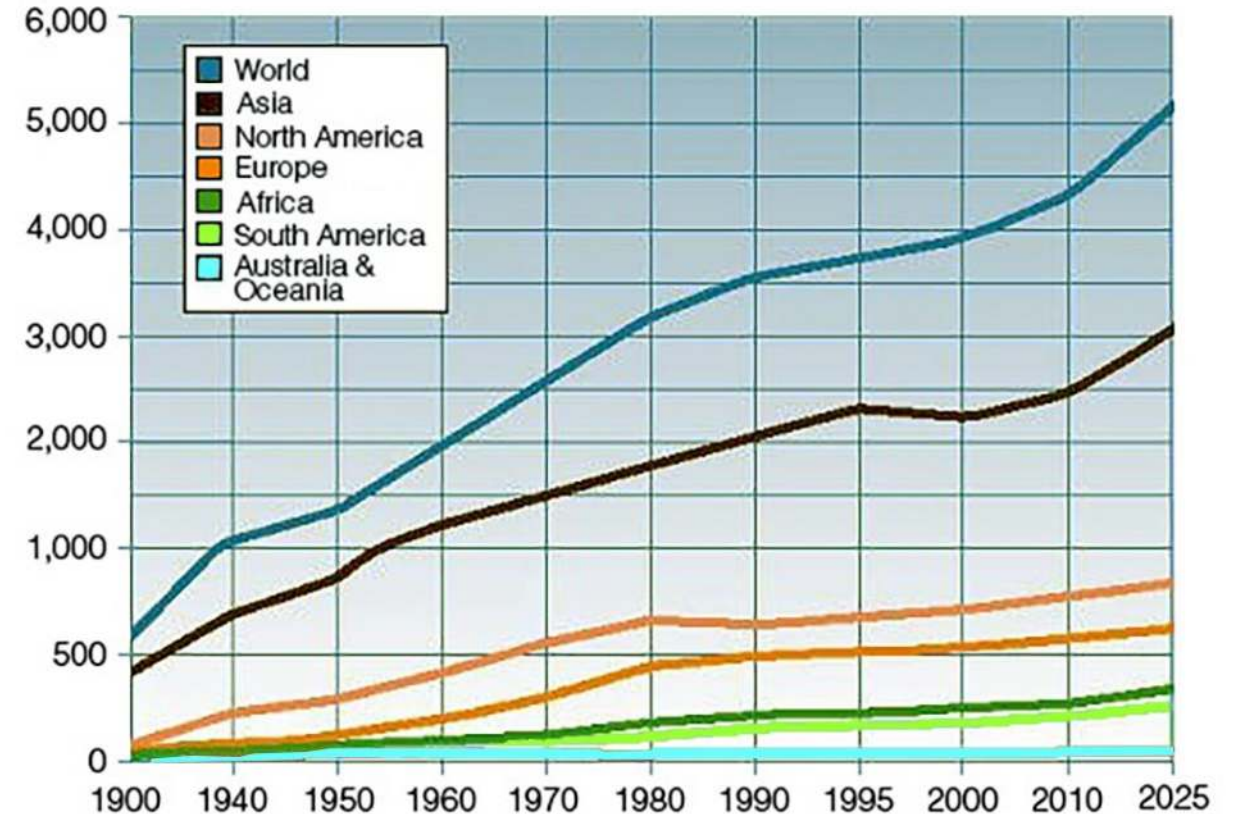
- Very small percentage of the total water available is freshwater
- Yet, we depend on freshwater for our municipal, agricultural and industrial processes



Source: Legacy Water Foundation, 2018

## Global Water Consumption 1900 – 2025

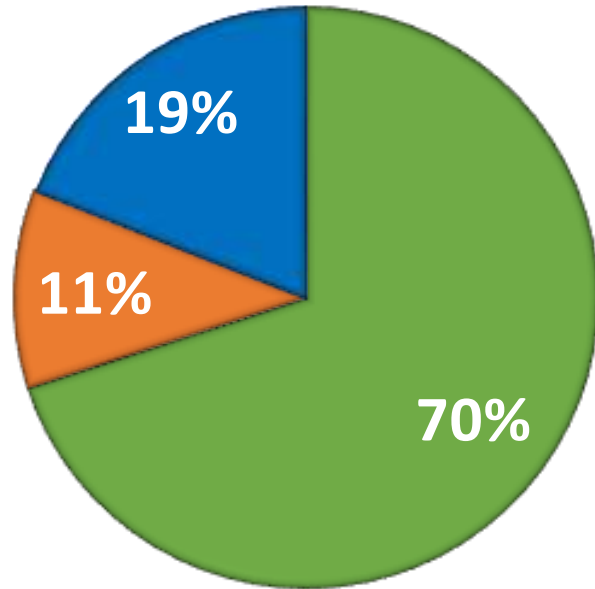
(by region, in billions of m<sup>3</sup> per year)



Source: [https://en.wikipedia.org/wiki/Water\\_scarcity](https://en.wikipedia.org/wiki/Water_scarcity)

# Freshwater Usage Data

Current freshwater usage statistics (2018)



■ Agricultural   ■ Municipal   ■ Industrial

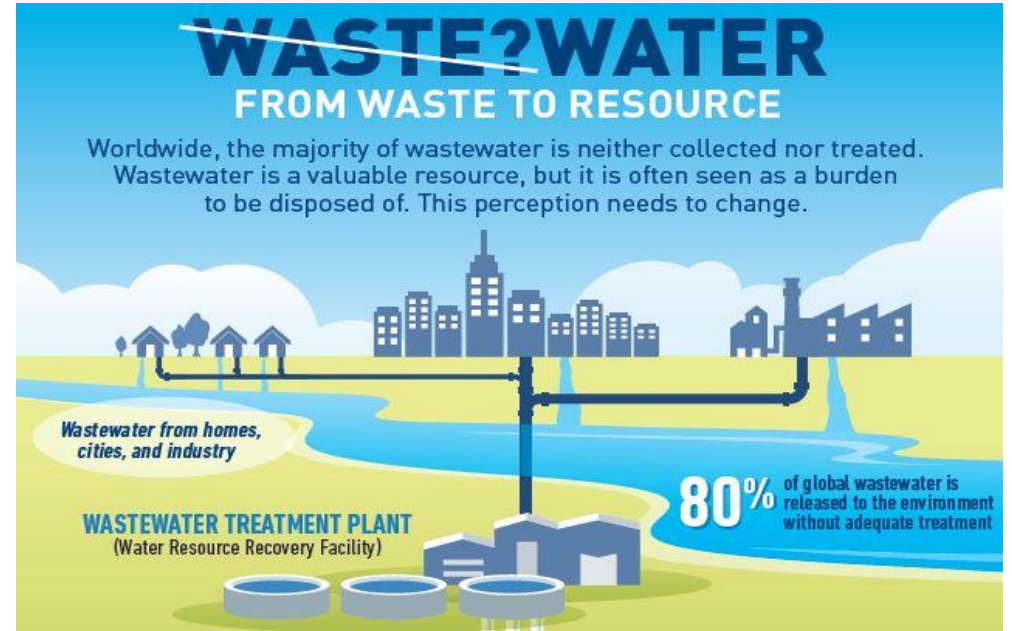
Projected freshwater usage in 2030



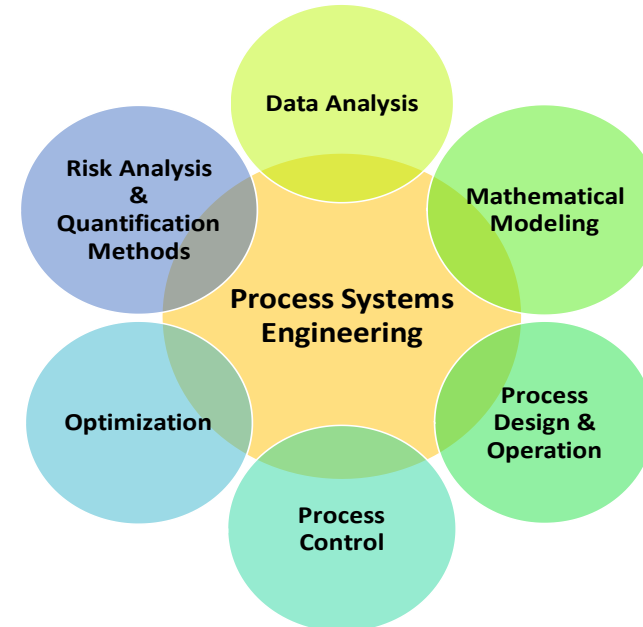
*Where will this additional 20% come from?*

# Solution.....?

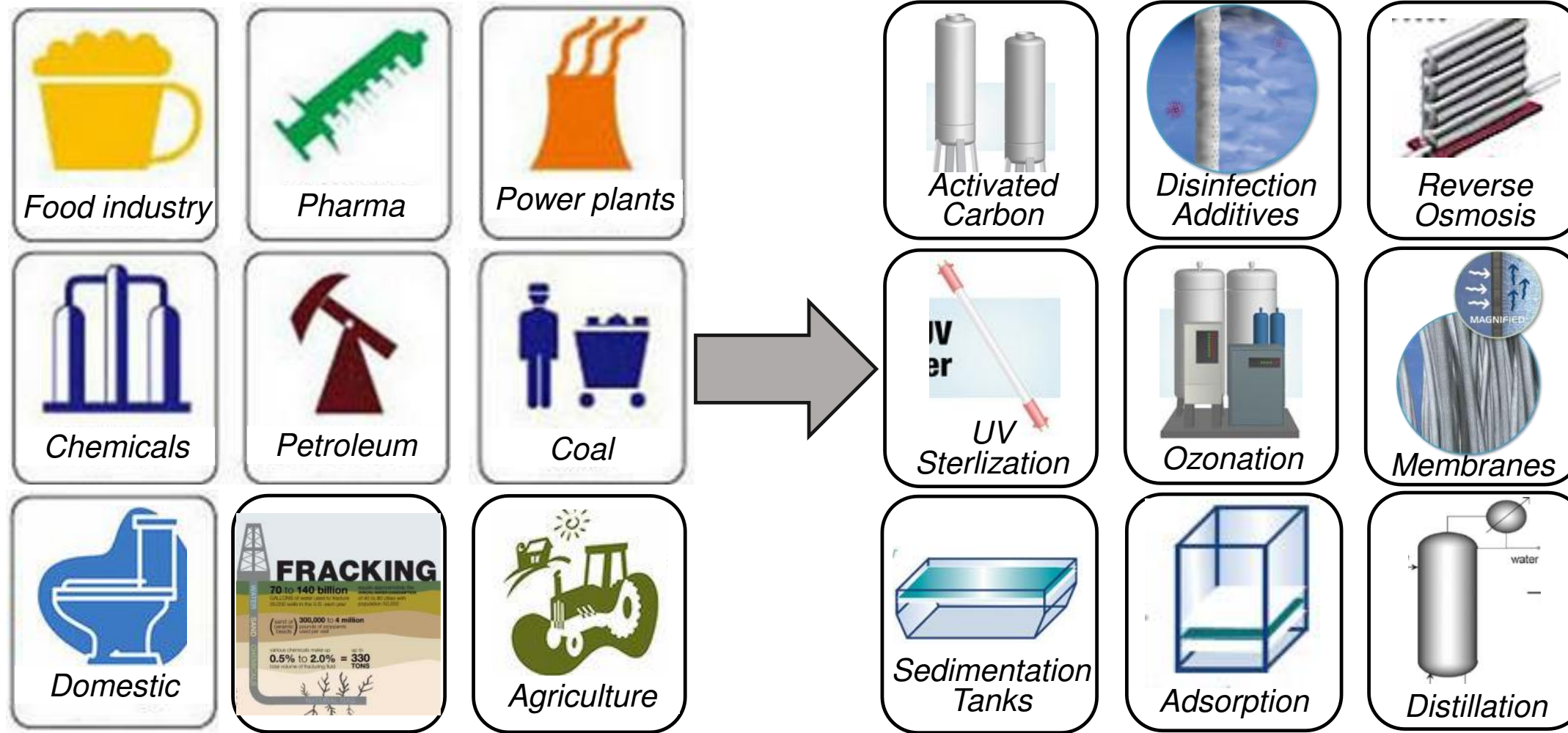
- To meet the demand we have to rely on **treated and recycled** water
- Thus, we need **efficient wastewater treatment methods** today to satisfy demands for sustainable existence tomorrow
- **Systems Engineering** can help in providing sustainable and cost effective insights



<https://blogs.worldbank.org/water/wastewater-treatment-critical-component-circular-economy>



# Wastewater Treatment: A Systems Problem

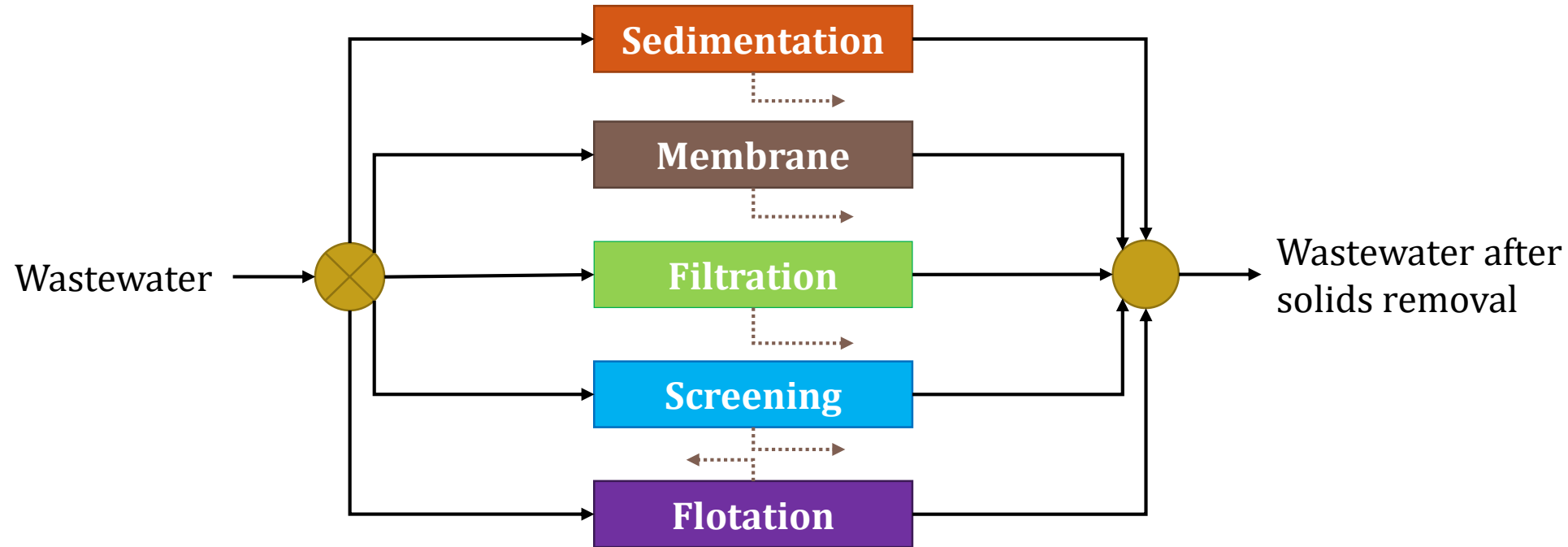


**Sources of Wastewater**

**Treatment Methods**

# Designing a Treatment Process

**Solids removal** is one of the tasks in Wastewater Treatment



## Complexity of the design problem

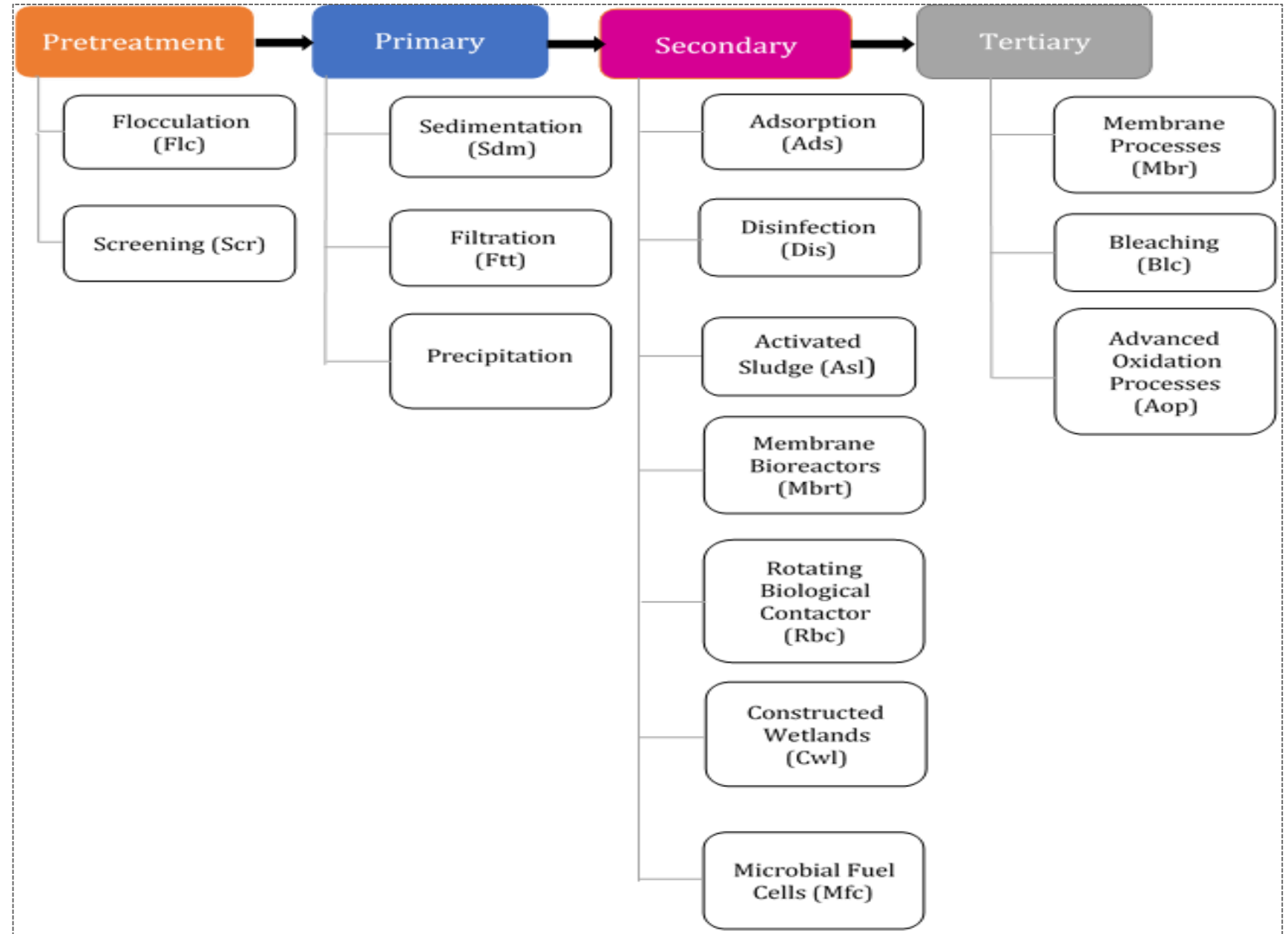
If a wastewater stream has  $C$  contaminants and  $S$  technologies for each task, then number of distinct treatment networks ( $N_f$ ) possible is given by

$$N_f = \frac{[2(C - 1)]! S^{(C-1)}}{C! (C - 1)!}$$

*If  $C = 5$  and  $S = 10$ , then  $N_f = 1.4 \times 10^5$  (close to a million) possible networks*

# Treatment Stages & Technologies

- Wastewater treatment is most effective using a stage-wise approach
- Technologies are placed in stages based on their contaminant removal capability







# Technology Information

Technology	Driving Force	Process conditions
<b>Sedimentation (Sdm) or Decantation (Dct)</b>	Density gradient Particle settling velocity	Size, density of particle Tank depth Residence time
<b>Filtration (Ftt)</b>	Particle size	Average flux, Pressure gradient Filtration rate
<b>Advanced Oxidation Process (Aop)</b>	Oxidation reactions for contaminant degradation	Ozone, peroxide, UV reactor
<b>Disinfection (Dis)</b>	Chemical, radiation	Chlorine dosage, Acid/Alkali treatment, UV radiation
<b>Rotating Biological Contactors (Rbc)</b>	Biological mechanism	Biological film on rotational discs, speed of rotation, aeration rate
<b>Membranes (Mbr)</b>	Particle/molecular size Sorptions/Diffusion Pressure	Pore size, Mol. wt. cut-off Average flux, Pressure gradient Type of membranes - MF, UF, NF and RO
<b>Activated Sludge (Acs)</b>	Microbial activity	Detention time, mixing efficiency, aeration rate



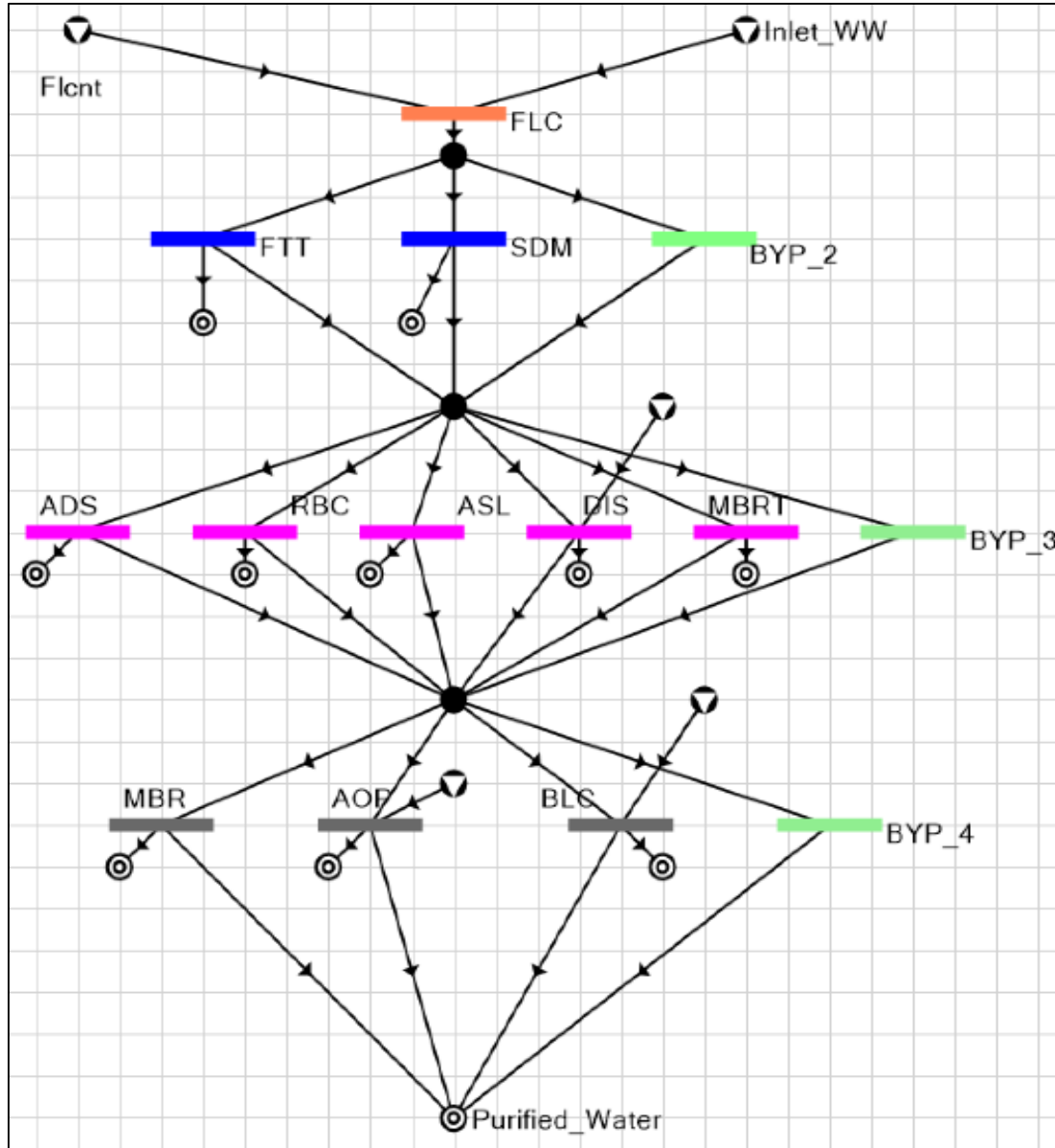
# P-graph Methodology

- P-graph (process graph) studio uses vertices and nodes to represent materials & operating units connected by arcs represent streams
- Includes two types of nodes
  - ✓ M-type: Materials  
raw materials ; products  & intermediates 
  - ✓ O-type: Operating units 
- Based on axioms for structurally feasible process networks
- Algorithms available:
  - ✓ MSG (Maximal Structure Generator): generates the maximal structure
  - ✓ SSG (Solution-Structure Generator): generates all the structurally feasible process networks
  - ✓ ABB (Accelerated Branch and Bound): generates the optimal or n-best feasible networks

# Stage-wise Wastewater Treatment Superstructure

## Key:

Pretreatment;  
Primary  
Treatment;  
Secondary  
Treatment;  
Tertiary  
Treatment;  
Bypass



Superstructure Generated: P-Graph

## What is a superstructure?

It is a systematic representation of all possible treatment technologies available in the 4 stages of wastewater treatment.

It also shows the flow from the initial wastewater stream towards the final purified water stream

FLC - Flocculation, SDM - Sedimentation, FTT - Filtration, ADS - Adsorption, RBC - Rotating Biological Containers, ASL - Activated Sludge, DIS - Disinfection, MBRT - Membrane Bioreactor, MBR - Membrane Processes, AOP - Advanced Oxidation Processes, BLC - Bleaching, BYP - Bypasses

# Framework for Design & Evaluation

- Provide input wastewater composition and define output purity specifications
- Construct the wastewater treatment network design as an optimization model
  - ✓ Mass and energy balances
  - ✓ Investment and Operating Costs
  - ✓ Integer variables to select technologies by holding a (0,1) value
- Method: **P-Graph Studio** (Graph Theory based Process Synthesis);  
MILP (Mixed integer linear programming) solver

# Case Study: Municipal Wastewater Treatment

Entering flowrate of wastewater in the treatment system: 100 m<sup>3</sup>/hr

Operating days per year: 330

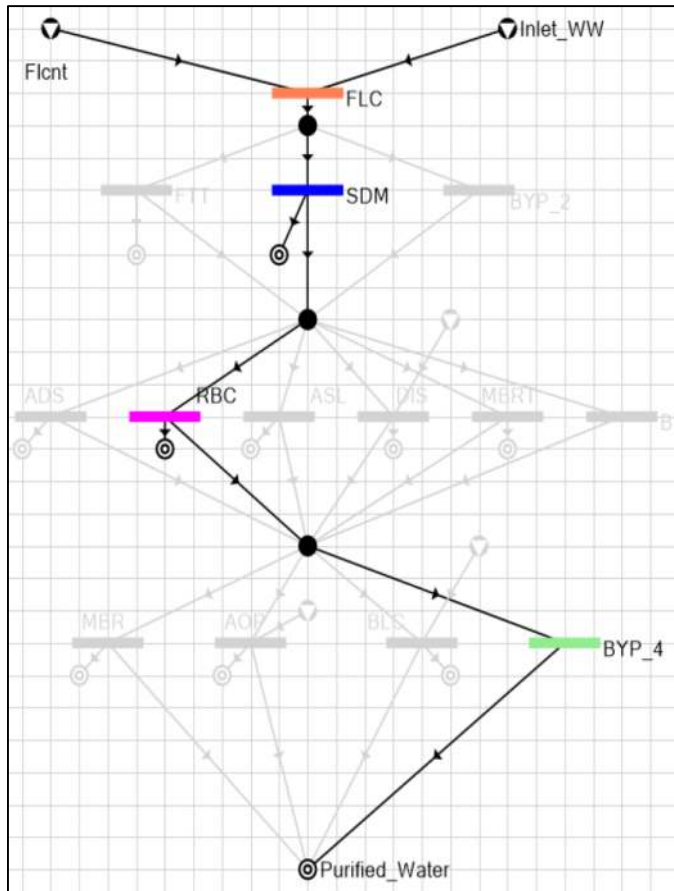
## Wastewater contaminant concentrations and purity levels

Contaminant	Inlet Amount	Outlet Amount	Units
Acids/Chlorides	5000	300	mg/L
COD (Inorganic)	2000	70	mg/L
BOD (Organic)	1100	25	mg/L
Settable solids	200000	500	mg/L
Metals (Pb, Cu, Ni, Zn)	1340	5	µg/L

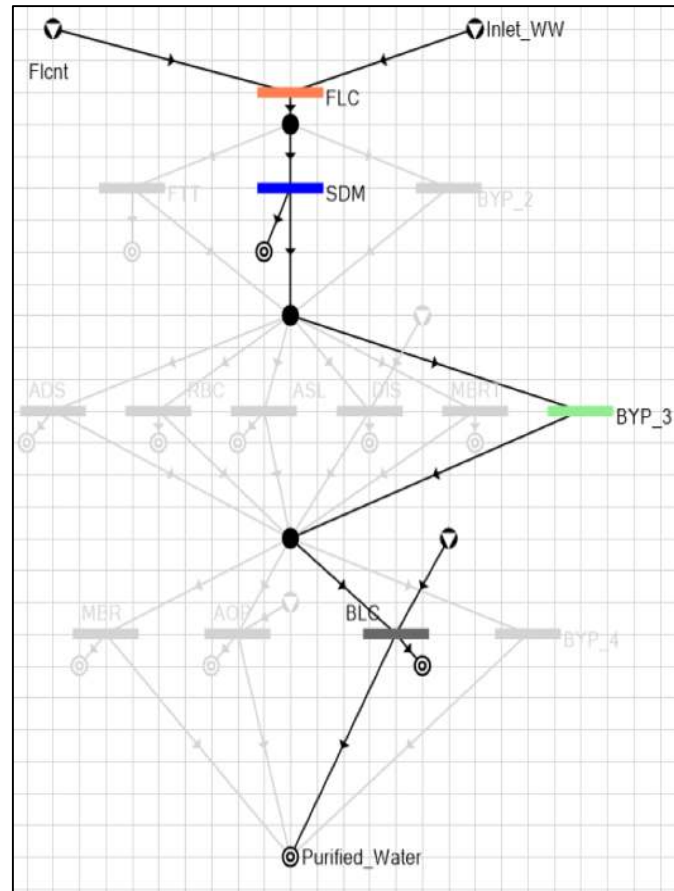
Source: Page et.al., 1996 "Use of Reclaimed Water and Sludge in Food Crop Production", The National Academy Press for publications in Sciences, Engineering and Medicine.

# Solutions from P-Graph formulation

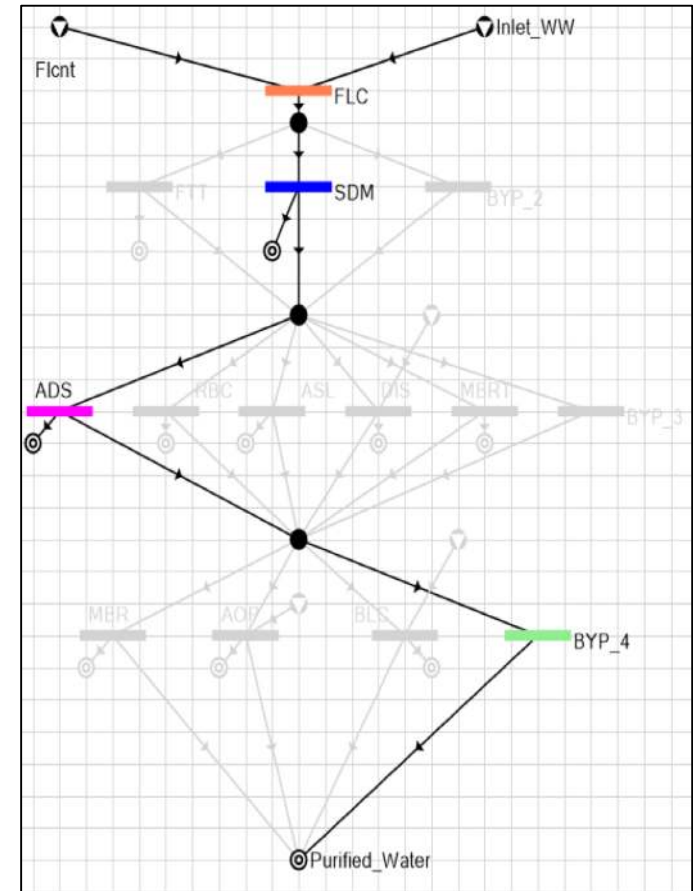
- ❖ The total best network solution generated using the P-Graph approach is 45 with a solution time of 0.035 seconds
- ❖ Costs: Fix and Proportional Investment Costs, Fix and Proportional Operating Costs



- Feasible Structure 1: (FLC-SDM-RBC)
- Purification Cost (\$/yr.) : 3197040



- Feasible Structure 2: (FLC-SDM-BLC)
- Purification Cost (\$/yr.) : 3256250



- Feasible Structure 3 (FLC-SDM-ADS)
- Purification Cost (\$/yr.) : 3901470

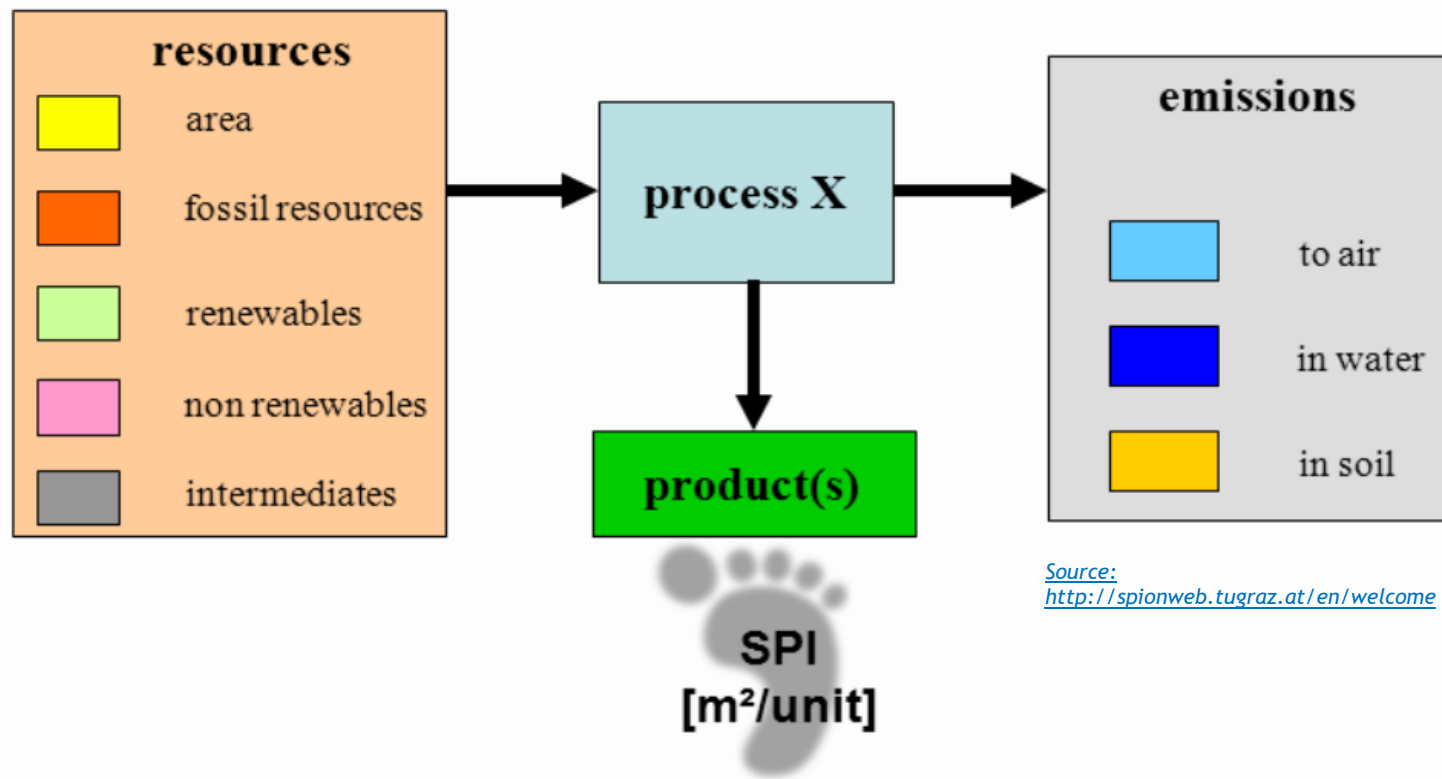
# Solutions from P-Graph formulation

Summary of the first best 10 feasible network pathways

No	Network Path	Purification Cost, (\$/yr)	Purification Cost/Liter of Purified Water(\$/L)
1	FLC-SDM-RBC	3197040	0.004249
2	FLC-SDM-BLC	3256250	0.004327
3	FLC-SDM-ADS	3901470	0.005185
4	FLC-FTT	4447680	0.005637
5	FLC-SDM-RBC-BLC	4507400	0.005990
6	FLC-SDM-AOP	4815100	0.006399
7	FLC-SDM-ADS-BLC	5343310	0.007101
8	FLC-FTT-RBC	5417120	0.007199
9	FLC-FTT-BLC	5482110	0.007286
10	FLC-SDM-RBC-AOP	6066250	0.008062

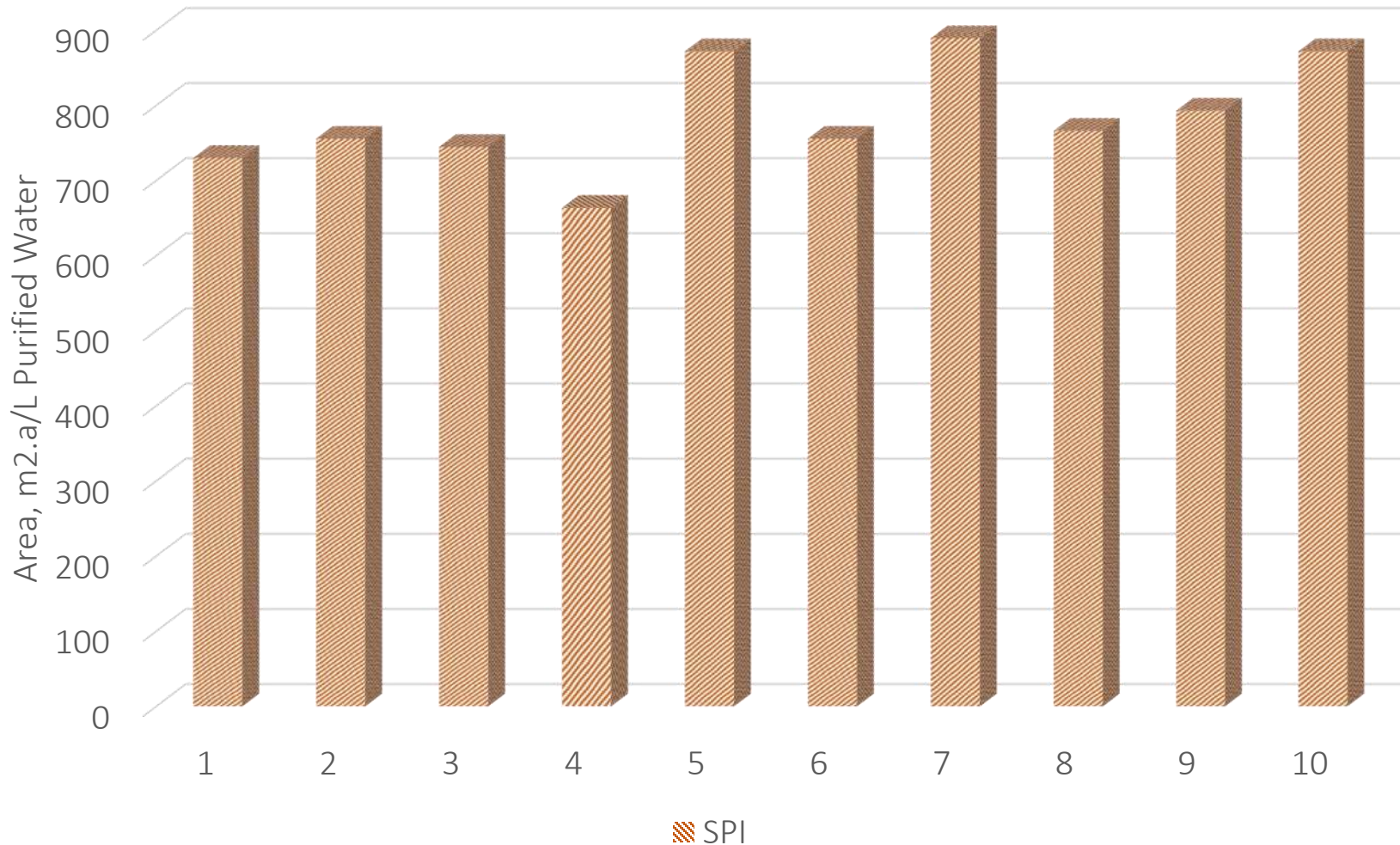
# The Sustainable Process Index (SPI)

- Ecological Footprint
- Quantification of sustainability based on arable area needed to produce one unit of product
- The burden of a process on the ecosystem
- The higher the SPI, the less sustainable the process is



# Solutions from SPI

- FLC-SDM-RBC-AOP (7) has the highest SPI Value
- FLC-FTT (4) has the lowest SPI Value



Index	Network Path
1	FLC-SDM-RBC
2	FLC-SDM-BLC
3	FLC-SDM-ADS
4	FLC-FTT
5	FLC-SDM-RBC-BLC
6	FLC-SDM-AOP
7	FLC-SDM-ADS-BLC
8	FLC-FTT-RBC
9	FLC-FTT-BLC
10	FLC-SDM-RBC-AOP



# Conclusions from P-Graph and SPI Analysis

- In terms of cost, network path (1) had the minimum, but network path (4) had had the lowest SPI value
- Even though network path (4) had the lowest SPI value, it was the only network path that could not meet purification requirements
- To make a decision, there should be trade-offs between cost and “greenness” of the process

# Summary

- ❖ An integrated approach involving design and optimization for generation of cost-effective wastewater treatment networks
- ❖ P-Graph approach to wastewater treatment using a superstructure optimization (MINLP)
- ❖ Generated a rank of network synthesis for wastewater treatment based on purification cost
- ❖ Sustainable process index (SPI) evaluation of generated synthesis paths



**Thank you for  
your attention!**